Chapter 10.

Step-Reaction and Ring-Opening Polymerization

10.2. Step-Reaction Polymerization - Kinetics

Step-Reaction Polymerization

- 1. Difunctional monomers \implies Linear polymers AB type, AA and BB
- 2. Polyfunctional monomers A Network polymers Functionality > 2
- 3. Polymers retain their functionality as end groups at the completion of polymerization

4. Single reaction (cf. initiation, propagation, and termination in chain-reaction polymerization)

5. M.W. increases slowly

Carothers equation

$$\overline{DP} = \frac{1}{1-p}$$
 p = extent of reaction

6. High-yield reactions and an exact stoichiometric balance are necessary to obtain high-m-w linear polymer

7. Formation of cyclic byproduct



Polymer Type	Repeating Functional Unit	Chapter	
Polyether	—Ar—O—	11	
Polyether [poly(phenylene oxide)]		11	
Polyether (epoxy) ^a	OH —CH₂ĊHCH₂OAr—	11	
Polysulfide	—ArS—	11	
Poly(alkylene polysulfide)	RS _x	11	
Polysulfone	—ArSO ₂ —	11	
Polyester		12	
Polycarbonate	0 	12	
Polyamide	O II —RCNH—	13	
Polyurea	O II —RNHČNH—	13	
Polyurethane	O II —ROČNH—	13	
Phenol–formaldehyde ^b	CH2	14	
Urea–formaldehyde ^c	O SNCNHCH₂—	14	
Melamine–formaldehyde ^b	N N CH_2	14	
Polyimide		15	

TABLE 10.1. Commercially Important Polymers Prepared by Step-Reaction Polymerization

Polymer Type	Repeating Functional Unit	Chapter	
Polybenzimidazole	- NH NH	15	
Polyphenylene		17	
Poly(p-xylylene)	-CH2-CH2-	17	

TABLE 10.1. (continued)

Kinetics of Step-Growth Polymerization Flory's assumption

The reactivity of a functional group is independent of the length of the chain to which it is attached.

Example: dibasic acid + glycol polyester



Assumption 2.

• The reactivity of a functional group is unaffected by reactions of other functional groups in the molecule

WAS FLORY RIGHT?

The probability of chemical reaction with the increase of the MW:

• The rate of molecular diffusion decreases, i.e., larger time intervals between encounters (fewer encounters of functional groups per unit time)

• Greater duration of each encounter (a larger number of collisions of functional groups per encounter)

- Kinetics
 - 1. Catalyzed [cat]k' = k [cat] is unchanged If polymerization reaction is first order w.r.t. each functional group (A & B)

 $\frac{1}{[A]} - \frac{1}{[A]_{o}} = kt$

 $\overline{\mathsf{DP}} = \frac{[\mathsf{A}]_{\mathsf{o}}}{[\mathsf{A}]} = \frac{1}{1-\mathsf{n}}$

By integration

$$\frac{1}{[A]_{o}(1-p)} - \frac{1}{[A]_{o}} = kt$$

$$\frac{\overline{\mathsf{DP}}}{[\mathsf{A}]_{\mathsf{o}}} - \frac{1}{[\mathsf{A}]_{\mathsf{o}}} = \mathsf{kt}$$

or

$$\overline{\mathsf{DP}} = [\mathsf{A}]_{\mathsf{o}}\mathsf{kt} + 1$$

$$\mathbf{t} = \frac{\overline{\mathbf{DP}} - \mathbf{1}}{[\mathbf{A}]_{\mathbf{o}}\mathbf{k}}$$

2. Uncatalyzed (self-catalyzed)

HOOC - COOH + HO – OH \rightarrow polymer

Carboxylic acid: role of catalyst

$$-\frac{d[A]}{dt} = k[A]^{2}[B]$$
Assume [A] = [B]
$$-\frac{d[A]}{dt} = k[A]^{3}$$

Integration

$$\frac{1}{[A]^2} - \frac{1}{[A]_o^2} = 2kt$$

[A] = [A]_o(1 - p)

$$\frac{1}{[A]_{o}^{2}(1-p)^{2}} - \frac{1}{[A]_{o}^{2}} = 2kt$$
$$\frac{1}{(1-p)^{2}} = 2kt[A]_{o}^{2} + 1$$
$$\overline{DP}^{2} = 2kt[A]_{o}^{2} + 1$$

M.W. increases more gradually than when acid catalyst is added.

t

10.3 Stoichiometric Imbalance

• Three ways to limit M.W. in step polymerization

1. To quench the polymerization reaction by rapid cooling when the desired M.W. is attained.

2. To use an excess of one monomer.

3. To use small amounts of monofunctional reactant

Stoichiometric imbalance factor

$$r = \frac{N_A^{o}}{N_B^{o}}$$

where

 N_A^o = initial # of A functional groups N_B^o = initial # of B functional groups

By convention

of molecular chains at p

r ≤ 1

p = extent of reaction =
$$\frac{N_A^{\circ} - N_A}{N_A^{\circ}}$$

N_A = (1 - p)N_A^o
N_B = (1 - pr)N_B^o = (1 - pr) $\frac{N_A^{\circ}}{r}$

$$N = \frac{1}{2} (N_{A} + N_{B})$$
$$= \frac{1}{2} \left[(1-p)N_{A}^{o} + (1-pr)\frac{N_{A}^{o}}{r} \right]$$
$$= \frac{N_{A}^{o}}{2} \left(1 + \frac{1}{r} - 2p \right)$$

cf. $N_{B} = N_{B}^{o} - pN_{A}^{o} = N_{B}^{o} - prN_{B}^{o}$

monomers

$$N^{\circ} = \frac{1}{2} \left(N_{A}^{\circ} + N_{B}^{\circ} \right)$$

Since $r = \frac{N_{A}^{\circ}}{N_{B}^{\circ}}$
 $N^{\circ} = \frac{1}{2} \left(N_{A}^{\circ} + \frac{N_{A}^{\circ}}{r} \right) = \frac{N_{A}^{\circ}}{2} \left(\frac{r+1}{r} \right)$

Average degree of polymerization

$$\overline{DP} = \frac{N^{\circ}}{N} = \frac{\frac{N^{\circ}}{2}\left(\frac{r+1}{r}\right)}{\frac{N^{\circ}}{2}\left(1+\frac{1}{r}-2p\right)} = \frac{1+r}{1+r-2rp}$$

lf r = 1

If p = 1

$\overline{\mathbf{DP}} = \frac{1}{1}$	$\overline{\mathbf{PP}} - \frac{1+r}{r}$
1 - p	$D_{1} = \frac{1}{1-r}$

If monofunctional reagent is added

Imbalance factor

$$r' = \frac{N_{A}^{o}}{N_{B}^{o} - 2N_{B'}^{o}}$$

where

N_B^{,o} = # of monofunctional B groups

Factor 2 : each B' molecule is equally as effective as one excess BB monomer in limiting the M.W.

10.4 M.W. Distribution

```
# of total molecules at p = N
# of x-mers = N_x
           M - (M)<sub>x-2</sub> - M
p p 1 - p
   where
         \begin{bmatrix} p = extent of reaction = probability of reaction \\ 1 - p = probability of finding an unreacted group \end{bmatrix}
 N_{x} = Np^{x-1}(1-p)
          \frac{N}{N^{o}} = 1 - p \qquad N_{o} = initial \ \# \ of \ monomers
  N_{x} = N_{a}(1-p)^{2}p^{x-1}
  n<sub>x</sub> = mole fraction of x-mers
 \mathbf{n}_{x} = \frac{\mathbf{N}_{x}}{\mathbf{N}} = (1 - \mathbf{p})\mathbf{p}^{x-1}
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p = 0.99

Monomer: the most abundant species

Wt fraction of x-mers

$$\mathbf{w}_{x} = \frac{\mathbf{x}\mathbf{N}_{x}\mathbf{M}_{o}}{\mathbf{N}_{o}\mathbf{M}_{o}} = \frac{\mathbf{x}\mathbf{N}_{x}}{\mathbf{N}_{o}} \qquad \qquad \text{cf.} \quad \mathbf{N}_{x} = \mathbf{N}_{o}(1-p)^{2}p^{x-1}$$

where $M_o = mass of repeating unit$

Wt fraction distribution

$$\mathbf{w}_{\mathbf{x}} = (\mathbf{1} - \mathbf{p})^2 \mathbf{x} \mathbf{p}^{\mathbf{x}-1}$$

The most abundant species

$$\frac{dw_{x}}{dx} = (1-p)^{2}p^{x-1} + (1-p)^{2}xp^{x-1}\ln p$$
$$= (1-p)^{2}p^{x-1}(1+x\ln p) = 0 \qquad \qquad x = -\frac{1}{\ln p}$$

$$\begin{split} \overline{M_n} &= \sum n_x M_x = \sum n_x x M_o = M_o (1-p) \sum x p^{x-1} = M_o (1-p) \frac{1}{(1-p)^2} = \frac{M_o}{1-p} \\ & \text{cf.} \quad \sum_{x=1}^{\infty} x p^{x-1} = \frac{1}{(1-p)^2} \end{split}$$

$$\overline{M_{w}} = \sum w_{x}M_{x} = \sum w_{x}xM_{o} = M_{o}(1-p)^{2}\sum x^{2}p^{x-1} = M_{o}(1-p)^{2}\frac{1+p}{(1-p)^{3}} = \frac{M_{o}(1+p)}{1-p}$$
cf.
$$\sum_{x=1}^{\infty} x^{2}p^{x-1} = \frac{1+p}{(1-p)^{3}}$$

Polydispersity index

$$\frac{M_{w}}{\overline{M_{n}}} = 1 + p$$

As
$$p \rightarrow 1$$
, $\frac{M_w}{\overline{M_n}} \rightarrow 2$

Fig 10.1 Mole fraction distribution in linear step-reaction polymerization

Fig 10.2 Weight fraction distribution in linear step-reaction polymerization

Theory of Gelation

Polycondensation of
$$A - A + A - \begin{pmatrix} A \\ A \end{pmatrix} + B - B$$

10.5 Network Step Polymerization

Equimolar mixture

Average functionality	f $-\frac{2+3+2+3}{2}-25$			
Average functionality	$I_{av} = \frac{1}{4}$			

- $N_o = initial # of monomers$
- N = # of molecules at p

of functional groups reacted = $2(N_o - N)$

Initial # of functional groups = $N_o f_{av}$

$$p = \frac{2(N_o - N)}{N_o f_{av}} = \frac{2}{f_{av}} - \frac{2N}{N_o f_{av}} = \frac{2}{f_{av}} - \frac{2}{\overline{DP}f_{av}} \qquad \text{cf.} \quad \overline{DP} =$$

N_o N

At gel point $\overline{DP} = \infty$

$$p_c = \frac{2}{f_{av}}$$
 Critical extent of reaction

If $f_{av} = 2.5$, $p_c = 80\%$ (cf: difunctional monomers : $\overline{DP} = 5$)

If mixture 3 mol of 1, 2 mol of 4

$$f_{av} = \frac{(3 \times 2) + (2 \times 3)}{5} = 2.4$$

$$p_{c} = \frac{2}{2.4} = 83\%$$

A - AB - B A_f # of molecules N_A N_B N_C Functionality $f_A = 2$ $f_B = 2$ $f_C = f > 2$

Imbalance factor

$$r = \frac{f_A N_A + f_C N_C}{f_B N_B} = \frac{2N_A + f_C N_C}{2N_B} \qquad \rho = \frac{f_C N_C}{f_A N_A + f_C N_C} = \frac{f_C N_C}{2N_A + f_C N_C}$$

 p_A = extent of reaction for A

 p_B = extent of reaction for B = rP_A

 $\begin{array}{lll} A_{f-1} - A - \left[B - B \ A - A \right]_{i} - B - B \ A - A_{f-1} \\ & p_{A} & (p_{B}(1 - \rho)p_{A})^{i} & p_{B}\rho \\ & = (r \ (1 - \rho)p_{A}^{2})^{i} & = r\rho p_{A} \end{array}$

Branching probability

= probability that a functional group on a branch unit leads to another branch unit

$$\alpha = \sum_{i=0}^{\infty} \mathbf{p}_{A} \left[\mathbf{r} (\mathbf{1} - \rho) \mathbf{p}_{A}^{2} \right]^{i} \mathbf{r} \rho \mathbf{p}_{A} = \frac{\mathbf{r} \rho \mathbf{p}_{A}^{2}}{\mathbf{1} - \mathbf{r} (\mathbf{1} - \rho) \mathbf{p}_{A}^{2}}$$

Trifunctionally branched network polymer

i th envelope

Y_i branch points on the i th envelope

of branch points on (i + 1) th envelope

 $Y_{i+1} = 2 Y_i \alpha$

Criterion for gelation

 $\alpha_{c} = critical branching probability = \frac{1}{f-1}$

$$\frac{1}{f-1} = \frac{r \rho {p_c}^2}{1-r(1-\rho){p_c}^2}$$

1 - r (1 - ρ) p_c^2 = (f - 1) r ρp_c^2

1 = (r - r ρ + f r ρ - r ρ) p_c^2

$$\mathbf{p_{c}} = \frac{1}{\left[\mathbf{r} + (\mathbf{f} - \mathbf{2})\mathbf{r}\rho\right]^{\frac{1}{2}}}$$

If r = 1

$$p_{c} = \frac{1}{\left[1 + (f - 2)\rho\right]^{\frac{1}{2}}}$$

If $\rho = 1$ No A - A All A_f $p_c = \frac{1}{[(f-1)r]^{\frac{1}{2}}}$ $p_c = \frac{1}{(f-1)^{\frac{1}{2}}}$

Theoretocal (statistical)

Carothers equation (nonstatistical)

$$p_{c} = \frac{1}{(3-1)^{\frac{1}{2}}} = \frac{1}{\sqrt{2}} = 0.707 \qquad f_{av} = \frac{(3 \times 2) + (2 \times 3)}{5} = 2.4$$

$$\alpha_{c} = p_{c}^{2} = \frac{1}{f-1} = \frac{1}{2} \qquad p_{c} = \frac{2}{f_{av}} \qquad p_{c} = \frac{2}{2.4} = 83\%$$

Experimental values of p_c fall between the values calculated by statistical and nonstatistical methods.

Deviation from statistical method

(1) Intramolecular branching reactions leading to wasted loops
 (2) Differing reactivities of the functional groups

Reactivity of secondary alcohol < Reactivity of primary alcohol In glycerol

10.6 Step-Reaction Copolymerization

AA : BB : CC = 1 : 1 : 2 Random copolymer

BB $AA + 2 CC \implies CC - AA - CC \implies - (CC - AA - CC - BB) -$

Alternating copolymer

Step polymers : true telechelic polymers

HO—polyether—OH + OCN—polyurethane—NCO ----

ABA triblock copolymer

10.7 Step Polymerization Techniques

1) Bulk polymerization

Free of contaminants

Disadvantage: high viscosity; elevated temp for effective stirring and removal of byproducts

High vacuum to remove byproducts

2) Solvent polymerization

Low viscosity

Removal of byproduct by azeotropic distillation Removal of water in situ by use of effective dehydrating agent

Necessity of removing solvent

3) Interfacial polymerization

Solutions of two monomers in separate, immiscible solvents (one usually water)

Polymer is formed at the interface

e.g., Schotten – Baumann synthesis

"nylon rope trick"

Rapid stirring to maximize the interfacial area increases the yield of polymer

Characteristics of interfacial polymerization

(1) Reaction goes rapidly at low temp.

(2) Reaction is so rapid, diffusion of monomer to the interface is rate determining

(3) Monomer reacts with the growing chains at the interface more rapidly than it diffuses through the polymer film to initiate new chains; hence M.W.s tend to be significantly higher.

(4) An exact stoichiometric balance is not necessary.

Interfacial polymerization: the "nylon rope trick"

4) Phase-transfer catalysis (PTC)

Aqueous phase and **organic** phase

Catalyst: quarternary ammonium salt

Function by transporting a nucleophilic monomer from the aqueous phase to organic phase, where its nucleophilicity is greatly enhanced because of reduced solvation effects

organic phaseaqueous phase \leftrightarrow organic phaseCIH2CCH2CI+ NC-CH2COOC(CH3)3

organic phase

Q⁺ transfers anion **Y**⁻ into the organic phase as [**Q**⁺, **Y**⁻], which then react with an alkyl halide **R**X to give the substitution product **R**-**Y**

The produced Q⁺X⁻ is rapidly reconverted into Q⁺Y⁻ by anion exchange with nucleophile M⁺Y⁻ from the aqueous phase.

10.8 Dendritic Polymers

- Potential applications: drug delivery systems, controlled release of agricultural chemicals, molecular sensors, rheology modifiers
- Characteristic features of dendrimers
 - 1. Three component parts: a central core, an interior dendritic structure, and an exterior surface
 - 2. Macromolecular dimensions are easily controlled by a repetitive sequence of synthetic steps.
 - 3. More soluble than linear polymers
 - ∵ High surface functionality
 - 4. Lack of chain entanglement → Low viscosity
 - 5. Supramolecular assemblies by incorporating guest molecules among the interior branches of the dendrimer.

Two approaches to construct dendrimers

1. Divergent synthesis

Branch points are constructed in a stepwise fashion from a central core.

2. Convergent synthesis

Branch segments are constructed separately and then joined to a multifunctional core.

Divergent synthesis

Polyamidoamine (PAMAM) dendrimers

 $NH_3 + 3 CH_2 = CH - COOCH_3 \longrightarrow N(CH_2CH_2COOCH_3)_3$

10th generation

of surface functional groups = $3 \times 2^{10} = 3072$

Surface area: 100 times

Convergent synthesis

Scheme 10.3 Convergent synthesis of a dendrimer from dendritic segments.

Hyperbranched polymers

More random architectures and do not emanate from a central core.

Synthesized from AB_x functional monomers

Polymerization occurs via dendritic branching with no possibility of crosslinking

Random Branching Without Network Formation

Polycondensation of the monomer $A-R-B_2$. Note that each x-meric species contains (x + 1) unreacted B groups and only one A group.

Similarly for addition of A-B

Essentially the same structure

But if A—A, or (A—A + B—B) added: infinite structures are possible!

10.9 Ring-Opening Polymerization

- Mechanisms
 - 1. Monomer is attacked by ionic or coordination species (X*)

2. Monomer is attacked by X* — Coordination species

Reactivity from ring strain

3 > 4 > 8 > 7 > **5** > **6**

6-membered cyclic esters (lactones) \longrightarrow polyesters

6-membered cyclic amides (lactams) → polyamides

5-membered cyclic esters (lactones) → polyesters

5-membered cyclic amides (lactams) ---- polyamides

Cyclic ethers

Reactivity

Polyesters

Ring-Opening Polymerization of N-Carboxy Anhydrides

The product polymer is a poly(amino acid) or polypeptide or synthetic protein. This particular reaction is noteworthy because it is a chain reaction that occurs with expulsion of a small molecule (CO_2) . Such reactions are very rare.

Silicones

An example of an polymer with an inorganic backbone that can also be made by step polymerization.

Polyphosphazenes

An example of a completely inorganic polymer that can be functionalized with organic groups after polymerization.

Polymer Type	Polymer Repeating Group	Monomer Structure	Monomer Type	Chapter	
Polyalkene	olyalkene -{CH=CH(CH ₂) _x }-		Cycloalkene	8	
Polyether	{CH₂O}	°,	Trioxane	11	
Polyether	{(CH ₂) _x O}	(CH ₂) _x O	Cyclic ether ^a	11	
Polyester ^b $- \left[\begin{array}{c} 0 \\ (CH_2)_x CO \right] - \right]$		(CH ₂),	Lactone	12	
Polyamide $- \left[\begin{array}{c} 0 \\ (CH_2)_x CNH \right] + \left[\begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 $		(CH ₂), NH	Lactam	13	
Polysiloxane $\begin{bmatrix} CH_3 \\ I \\ SiO \\ I \\ CH_3 \end{bmatrix}$		[\$i(CH ₃) ₂] _x	Cyclic siloxane	16	
Polyphosphazene $\begin{bmatrix} CI \\ P=N \\ I \\ CI \end{bmatrix}$			Hexachloro- cyclotriphos- phazene ^c	16	
Polyamine	-{CH ₂ CH ₂ NH}-	NH CH ₂ —CH ₂	Aziridened	17	

TABLE	10.2.	Commercially	Important	Polymers	Prepared b	y Ring	g-Opening	Pol	ymerization

^aEpoxide (x = 2); oxetane (x = 3).

^bRing opening of cyclic oligomers has also been developed.

^cPhosphonitrilic chloride trimer.

^dAlso called alkyleneimine.